## **AMENDMENTS TO THE SPECIFICATION**

Please amend the specification as noted in the following paragraph from page 2, lines 12 to 21, at one location:

In a typical example system, a well produces a volume of liquids with some associated gas, for example,  $50\text{m}^3/\text{hr}$ . The pressure available for use by the cyclone de-sander is typically 1bar. Cyclone liner design characteristics determine that the efficient maximum flow rate per liner whilst meeting its  $d_{90}$  cut size is given by the available pressure drop allowed divided by a constant depending on the cyclone shape size and efficiency. In this example a cyclone liner is chosen that has a maximum flow rate under these conditions of  $10\text{m}^3/\text{hr}$  whilst separating 90% of all particles 20 microns and above that have a density equal to or greater than 2000 kg/m³. The field's initial flow rate is considered to be  $30\text{m}^3/\text{hr}$  and after one years year's operation is likely to increase to  $50\text{m}^3/\text{hr}$ .

Please amend the specification as noted in the following paragraph from page 10, lines 15-23, at one location:

The inner cyclone liner 16 should be displaced to the inoperative position when the cyclone separator 40 witnesses a high pressure drop across the system that indicates that the inner cyclone liner 16 taking the flow is too small or has insufficient area or volume for the unit to pass the incoming flow rate, whilst maintaining the required separation efficiency at the designed pressure drop. When in the inoperative position, the inner cyclone line liner 16 does not interfere with the flow through the larger outer cyclone liner 14. The effect is to decrease the pressure drop through the cyclone separator or de-sander to acceptable levels whilst maintaining desired flow rates and separation efficiencies.